

MAERZ OFENBAU AG

Is it sufficient to use renewable energy sources for lime kilns to achieve the climate goals?

Introduction

Climate change is becoming more and more noticeable, which is why global warming should be limited to 1.5 °C as already targeted by the Paris Climate Agreement in 2015. To achieve this goal, we must eliminate all CO₂ emissions into the atmosphere by 2050. Since this is not possible in one single step, various procedures and laws have already been put into effect, which now have to be systematically implemented. The industry is facing major chal-

lenges: on the one hand, when new plants are built, it must be ensured that the future emission targets are met and, on the other hand, these targets should also be met in the existing production plants. The use of renewable energy sources is a measure that can help to achieve the emission targets.

What are renewable energies?

Renewable energies, also known as regenerative energies, are energy sources that are either available

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in practically unlimited amounts or can grow back again in a relatively short period of time – in contrast to fossil fuels such as coal or natural gas. Renewable energy sources include hydropower, solar and wind power, and sustainably managed biomass. Other renewable energy sources are:

- » Liquid fuels, sustainably produced from bio-
- » Hydrogen, produced with hydro, solar and wind energy
- » Fuel gases, produced by fermentation or by pyrolysis of biomass

Using renewable energy sources can reduce CO₂ emissions from lime kilns, but is this enough to meet the climate targets?

PFR lime kilns still represent the state of the art when it comes to energy efficiency in the production of high reactive lime. In a natural gas-fired PFR lime kiln, 0.96 t of CO₂ are produced for each ton

of lime. 20% of this amount comes from burning natural gas and 80% from calcination. When using biogenic or renewable fuels, CO2 emissions are reduced from 0.96 to 0.768 t per t of lime. This is a step in the right direction, leading to a short-term improvement, without the need to invest in a CCUS system immediately. However, in order to reach the final climate targets, the CO₂ from calcination will also need to be captured. Another advantage of renewable energy sources is that they create the basis for future CO₂-negative lime production. These are important considerations that should be taken into account, as the climate targets must be gradually achieved by 2050. In addition, the sales price for lime must be adjusted to climate-neutral manufacturing processes, and that will take time as well. The transition of the lime industry towards climate neutrality is a complex task, which can be achieved through a wide variety of measures. If they are available, it makes sense to convert existing lime

1 Firing system for solid renewable fuels



Fuel requirements:

80 % < 1.0 mm, 100 % < 3.0 mm Particle size: no long fibers and needles Particle shape:

Bulk density: $> 150 \text{ kg/m}^3$ Ash content: < 3 % < 15 % Water content: Calorific value: > 13 MJ/kg (lower)

Design of the firing system:

- Very accurate gravimetric fuel metering
- Distribution of fuel by means of one special rotary valve for each two burner lances
- Low density conveying with air to the burner lances
- Pressure-shock-resistant weighing hopper with agitator for all lime kiln sizes up to 800 t/d
- In-house development by Maerz Ofenbau AG

kilns to biogenic fuels now and add a CCUS system later. When building new lime kilns, however, care should be taken to select a kiln type that enables a cost-effective combination with a CCUS system. Possibilities for this have already been published in ZKG 6-2021 [4].

Which biogenic fuels can be used for PFR lime kilns and what are the effects on the burning process?

Compared to the cement industry, the use of biogenic fuels in lime shaft kilns is limited. Sustainable fuels can contain high levels of ash or substances that have a negative impact on lime quality, or pollutant emissions. In contrast to the cement clinker process, the ash components are not bound in the clinker minerals, but they deteriorate the lime quality. There are also other aspects, which need to be considered.

In the case of solid biogenic fuels, the material must be crushed to the required grain size and, depending on the nature of the material, the energy required for this should not be underestimated. Depending on the water content, such fuels must also be dried. If the material is recycled, foreign material such as steel must be removed and harmful components must be burned in the lime kiln for a sufficiently long time at a sufficiently high temperature.

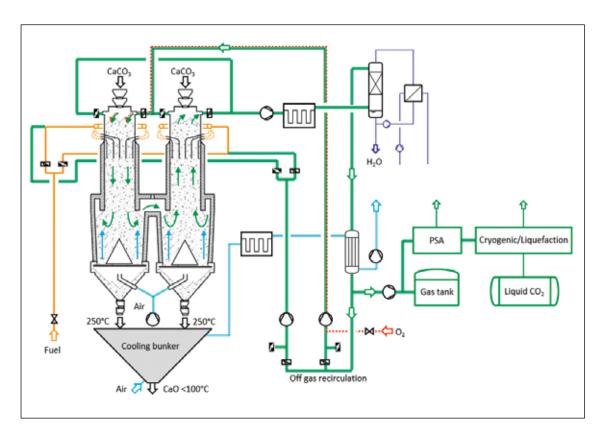
Regarding liquid biogenic fuels, the processing effort is usually limited to good filtration in order to separate any solids that would negatively affect the fuel dosing system. The availability of such fuels is rather limited and the fuels often come from food production, whereby the ethical aspects must also be taken into account. For any future synthetic liquid fuels, the price will probably be too

Table 1 Solid renewable energy sources for Maerz PFR lime kilns

Fuel	Calorific value [kJ/kg]	Consumption ^[5] [kg/t lime]	Density [kg/m³]	Pollutant emissions	To note	Effects on kiln operation ^[6]
Fresh wood[1]	13.2 to 16.0	231 to 285	150 to 270		- Impurities (e.g. glue, paint)	I, consumption - ~20% higher electric energy
Pellets from fresh wood	18.4	201	687 ^[2] 300 ^[3]	NO _x CO	Foreign matter (e.g. metal, plastics)	
Waste wood from the furniture industry	15.7 to 17.3	214 to 236	225 to 300	TOC Other	 Processing (crushing, drying, screening → approx. 100 kWh/t) 	
Torrefied biomass ^[4]	20.3	185	582		- Infrastructure (transport,	~20% higher off-gas volume
Bio char	16.2 to 19.8	187 to 228	345 to 436	unknown	storage)	at bag house filter inlet - ~20 °C higher kiln off-gas
Olive stones	19.8	187	648	NO _x	- Properties (flow behaviour,	
Almond shells	13.3	278	576	CO TOC	wear)	temperature
Bagasse	11.6	319	77	unknown	Sugar cane waste. Very light and therefore probably not usable.	

- [1] Brazil, Honduras, Mexico, Germany
- [2] Pellets as received
- [3] Pellets after disintegration in a hammer mill (estimated)
- [4] Torrefied olive remains
- [6] Consumptions apply to a specific heat demand of 3.7 MJ/t lime [6] Compared to a lignite fired PFR lime kiln

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2 Revamping of existing PFR lime kilns with oxyfuel firing and compared to amine scrubbing - inexpensive CO₂ separation and liquefaction

high, making them more viable for aviation. Figure 1 shows the proven "Maerz classic solid fuel dosing system" as an example, which is available for kiln sizes up to 800 t/d.

The use of gaseous biogenic fuels has numerous advantages and should definitely be considered. The biogases listed in Table 3 can be used directly in PFR lime kilns without much effort. With regard to pyrolysis gases, the gases usually contain a high proportion of tar. The tar must be separated beforehand, otherwise the compressor and dosing system would become clogged. Pyrolysis gases sometimes have a fairly low calorific value. With a calorific value of 3.0 to 4.5 MJ/Nm³, a PFR lime kiln could be converted according to [6]. Less effort is required for gases with a calorific value of more than 4.5 MJ/Nm3. In most cases, however, the gases have to be compressed and the fuel dosing systems have to be correctly dimensioned depending on the calorific value. Hydrogen will play an important role in the future and has the advantage that neither CO2 nor pollutant emissions are generated from combustion. Hydrogen can be used in PFR lime kilns without much effort and has no negative effects on the burning process and lime quality.

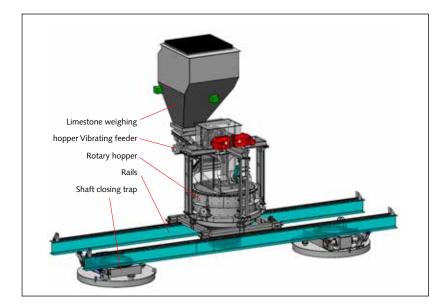
Taking into account decades of previous experience with PFR lime kilns, Tables 1 to 3 are intended to provide an overview of which biogenic fuels can be used for PFR lime kilns and how their use affects kiln operation, lime quality and pollutant emissions.

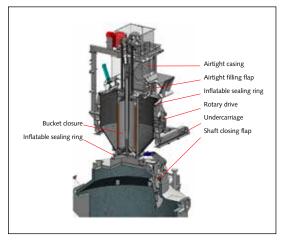
What measures are required to achieve economical CO2 separation on existing PFR lime kilns?

To all intents and purposes, an amine scrubber could be installed downstream. However, it must be noted that the energy demand for such a system is very high and the amine process is also sensitive in terms of health issues. The thermal energy requirement for an amine washing system would be about the same as the thermal energy requirement of the lime kiln itself.

For this reason, it could be advantageous to convert existing PFR lime kilns to oxyfuel firing.

3 Kiln charging system with rotary hopper combined with air lock system

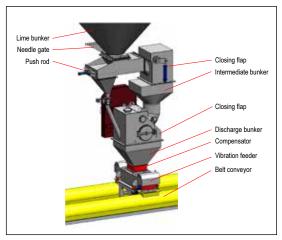




4 Rotary hopper with air lock system

With the method according to Figure 2, the amount of exhaust gas drops to around 50% and the CO2 concentration in the exhaust gas increases from 20% to almost 45%. This enables the use of a PSA gas separation system combined with a cryogenic system for purification and liquefaction of the CO₂. Such a system needs no chemical substances like amines or potassium carbonate, which could create health or corrosion problems. Both the investment and the operating costs of PSA-CRYO systems would be significantly lower than those with an amine scrubber, and both systems are harmless to health. The conversion of the firing process according to Figure 2 requires the following measures:

1. Installation of an air lock charging system in order to avoid dilution of the kiln off-gas with air. Figures 3 and 4 show an example for round PFR lime kilns. Such a system also allows charging the kiln with two different limestone



5 Air lock kiln discharge system

- grain sizes. This optimises the combustion and reduces the formation of CO and NO_x [1].
- 2. Installation of an air lock discharging system also in order to avoid dilution of the kiln offgas with air. Figure 5 shows an example, which is applicable to all lime shaft kilns.
- 3. Installation of an oxyfuel firing system. A mixture of recirculated kiln exhaust gas and oxygen is used to significantly reduce the nitrogen content in the combustion air. This process has already been published in [5], with the exception that the lime cooling air is not discharged from the kiln here, since existing lime shaft kilns were not designed for this. A high-pressure fan is used to compress the recirculation gases, please refer also to [7].
- 4. Since the downstream CO₂ capture system requires a continuous flow, a gas tank is needed to bridge the kiln reversal time.

Table 2 Liquid renewable energy sources for Maerz lime kilns

Fuel	Calorific value [kJ/kg]	Consumption ^[3] [kg/t lime]	Density ^[4] [kg/Nm ³]	Viscosity [cSt] ^[5]	Preheating temp. [°C]	Pollutant emissions	To note	Effects on kiln operation
Organic waste oil ^[1]	41.4	83	860	205 @ 40 °C 77 @ 60 °C 21 @ 100 °C	120		Tall oil is a product of pulp production in paper mills and will in future be used in a PFR kiln in Sweden.	No significant change
Vegetable oil ^[2]	37.8	90	920	74 @ 20 °C	40	co voc	Is mainly made from rapeseed and is therefore only available in limited quantities. In addition, politicians do not support the continued promotion of rapeseed oil for use in transport and industry.	
Biodiesel	37.0	92	880	7.5 @ 20 °C	Not re-		Is mainly made from grain, corn or sugar	
Bioethanol	37.0	127	776	<1.0 @ 20 °C	•		cane. Its low flashpoint of only 12 °C requires explosion protection measures.	
Synthetic fuels	The key figures are not yet available.						These fuels are still in the development phase and are not yet available.	

^[1] Pine oil or also called tall oil has a density of 938 kg/m³ @50°C

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^[2] The values in the table apply to rapeseed oil

^[3] Consumption applies to a specific heat requirement of 3.4 MJ/t lime [4] Reference temperature = 15 °C

 $^[5] cSt = mm^2/s$

Table 3 Gaseous renewable energy sources for Maerz lime kilns

Fuel	Calorific value [MJ/kg] [MJ/Nm³]	Consumption ^[6] [kg/t lime] [Nm³/t lime]	Density [kg/Nm³]	Pollutant emissions	To note	Effects on kiln operation ^[7]	
Biogas ^[1] 50 % CH ₄ 50 % CO ₂	13.3 18.0	255 190	1.347		ChlorineFluorineAmmoniaOther impurities	 ~3% higher thermal energy consumption ~10% higher electric energy consumption ~2 to ~3 times higher fuel volume to be injected 	
Biogas ^[1] 75 % CH ₄ 25 % CO ₂	26.0 26.9	130 126	1.032	60		 ~6% higher off-gas volume at bag house filter inlet ~20°C higher kiln off-gas temperature 	
Pyrolysis gas ^[3]	4.17 4.64	816 733	1.112	CO VOC	DustTarOther impurities	 ~9% higher thermal energy consumption ~2 times higher electric energy consumption ~8 times higher fuel volume to be injected ~1.5 times higher off-gas volume at bag house filter inlet >100°C higher kiln off-gas temperature 	
Biomethane ^[2] Syn. Methane ^[5]	50.0 35.9	68 95	0.718			No significant change	
Hydrogen ^[4]	119.9 10.8	28 315	0.09	none	Burning rate	 ~0.3% less thermal energy consumption ~20% less electric energy consumption ~3 times higher fuel volume to be injected ~5% less off-gas volume at bag house filter inlet ~0°C higher kiln off-gas temperature. 	

- [1] Gas from fermentation of plant and animal biomass or sewage treatment plants
- [2] Methane separated from biogas
- [3] Gas from pyrolysis of plant and animal biomass or sewage sludge (values in the table apply to pyrolysis gas from sewage sludge)
- [4] Made with hydro, solar or wind power [5] Made from sustainably produced H₂ and preferably CO₂ separated from off-gas
- [6] Consumption applies to a specific heat requirement of 3.4 MJ/t of lime [7] Compared to a natural gas fired PFR lime kiln
- 5. The lance cooling air has to be replaced by recirculated kiln off-gas.
- Optionally some of the existing lime kilns can discharge the product at higher temperatures [2] and the final cooling takes place outside of the kiln process in an after cooler. In such a case, the lime kiln would be operated with less lime cooling air, which further increases the CO₂ concentration in the kiln off-gases.

What is the best option when a new PFR lime kiln is needed?

For the most cost-effective CO₂ separation after the lime kiln, it is advantageous to have the CO₂ concentration in the kiln exhaust gas as high as possible. For this reason, the use of a Maerz EcoKiln® [5] or at least Maerz EcoKiln-ready is recommended, which would enable a simple subsequent conversion to oxyfuel firing and cooling air extraction (gas separation in the lime kiln). The second best option would be a PFR lime kiln with oxyfuel firing according to Figure 5.

Summary

Maerz Ofenbau AG has many years of experience in using renewable energies and can offer tailor-made solutions for the lime industry. However, since the sole use of biogenic fuels reduces CO2 emissions by only 20%, Maerz Ofenbau has also developed new lime shaft kilns and processes that enable cost-effective CO2 separation both for new and existing lime kilns. Since the CO₂ separation costs decrease sharply with increasing CO2 concentration in the kiln off gas, it is crucial to what extent the CO₂ concentration can be increased. Maerz Ofenbau has developed the new Maerz EcoKiln series for new installations, which can be operated with oxyfuel firing and separation of the lime cooling air inside the shaft kiln. However, these lime kilns can also be operated conventionally with air and without cooling air separation. In addition, Maerz has developed a process that makes it possible to operate existing lime kilns with oxyfuel firing, in which case the cooling air is not separated. In both cases, the otherwise required amine scrubbing can be replaced by other processes for final CO₂ separation that are harmless to health and significantly less energy-intensive.

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